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5.60 Thermodynamics & Kinetics Spring 2008

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Equilibrium in Solution

The chemical potential for molecules in solution is given by a formula that is very similar to that for ideal gases:

 $\mu_{\mathcal{A}}(\mathcal{T},\boldsymbol{p},\boldsymbol{c}_{\mathcal{A}}) = \mu_{\mathcal{A}}^{o}(\mathcal{T},\boldsymbol{p}) + \mathcal{RT}\ln\boldsymbol{c}_{\mathcal{A}} = \mu_{\mathcal{A}}^{o}(\mathcal{T},\boldsymbol{p}) + \mathcal{RT}\ln[\mathcal{A}]$

The precise definition of the standard chemical potential $\mu_A^o(T,p)$ is now more complicated; it is defined at a given pH, salt concentration, etc..., all solution properties that need to be defined in advance. We will not go through those and take it as a given that the standard state is appropriately defined.

Given a standard chemical potential $\mu^o_A(T,p)$, then the analysis that we did for the ideal gas follows straight through and we find for a solution process

$$v_A A(sol, T, p) + v_B B(sol, T, p) = v_C C(sol, T, p) + v_D D(sol, T, p)$$

that following the ideal gas analysis in our previous lecture

$$\Delta \mathcal{G}(\varepsilon) = \varepsilon \left\{ \left[v_{\mathcal{C}} \mu_{\mathcal{C}}^{\circ}(T) + v_{\mathcal{D}} \mu_{\mathcal{D}}^{\circ}(T) \right] - \left[v_{\mathcal{A}} \mu_{\mathcal{A}}^{\circ}(T) + v_{\mathcal{B}} \mu_{\mathcal{B}}^{\circ}(T) \right] + \mathcal{R}T \ln \left(\frac{\left[\mathcal{C} \right]^{v_{\mathcal{C}}} \left[\mathcal{D} \right]^{v_{\mathcal{D}}}}{\left[\mathcal{A} \right]^{v_{\mathcal{A}}} \left[\mathcal{B} \right]^{v_{\mathcal{B}}}} \right) \right\}$$

and the equilibrium constant K comes out through

$$\Delta \mathcal{G}_{rxn}^{o} = -\mathcal{RT} \ln \mathcal{K} , \qquad \mathcal{K} = \boldsymbol{e}^{-\Delta \mathcal{G}^{o}/\mathcal{RT}}$$

Where $K = Q_{eq} = \frac{[\mathcal{C}]^{\nu_{\mathcal{C}}}[\mathcal{D}]^{\nu_{\mathcal{D}}}}{[\mathcal{A}]^{\nu_{\mathcal{A}}}[\mathcal{B}]^{\nu_{\mathcal{B}}}}$ at equilibrium as before, and where the concentrations are equilibrium concentrations.

Temperature dependence of K (or K_p)

$$\ln \mathcal{K}(T) = -\frac{\Delta \mathcal{G}^{\circ}}{RT} \quad \Rightarrow \quad \frac{d \ln \mathcal{K}}{dT} = \frac{d}{dT} \left(-\frac{\Delta \mathcal{G}^{\circ}}{RT} \right) = \frac{\Delta \mathcal{G}^{\circ}}{RT^{2}} - \frac{1}{RT} \frac{d \Delta \mathcal{G}^{\circ}}{dT}$$

But at <u>fixed pressure and/or solutions properties</u> (*p* = 1 bar, pH constant, etc..)

$$\frac{d\Delta \mathcal{G}^{\circ}}{dT} = \left(\frac{\partial \Delta \mathcal{G}^{\circ}}{\partial T}\right)_{1 \text{ bar,pH constant, etc...}}$$

and from fundamental equation

$$d\mathcal{G} = -\mathcal{S}dT + \mathcal{V}dp \implies \left(\frac{\partial \mathcal{G}}{\partial T}\right)_{p} = -\mathcal{S} \implies \left(\frac{\partial \Delta \mathcal{G}^{\circ}}{\partial T}\right)_{p} = -\Delta \mathcal{S}^{\circ}(T)$$

$$\therefore \qquad \frac{d\ln K}{dT} = \frac{\Delta \mathcal{H}^{\circ}(T) - T\Delta \mathcal{S}^{\circ}(T)}{RT^{2}} + \frac{1}{RT}\Delta \mathcal{S}^{\circ}(T)$$

$$\boxed{\frac{d\ln \mathcal{K}(T)}{dT} = \frac{\Delta \mathcal{H}^{\circ}(T)}{RT^{2}}}$$

<u>Integrating</u>: $\ln \mathcal{K}(\mathcal{T}_2) = \ln \mathcal{K}(\mathcal{T}_1) + \int_{\mathcal{T}_1}^{\mathcal{T}_2} \frac{\Delta \mathcal{H}^{\circ}(\mathcal{T})}{\mathcal{R}\mathcal{T}^2} d\mathcal{T}$

At constant $p: \Delta \mathcal{H}^{\circ}(\mathcal{T}) = \Delta \mathcal{H}^{\circ}(\mathcal{T}_{1}) + \Delta \mathcal{C}_{\rho}(\mathcal{T} - \mathcal{T}_{1})$

$$\ln \mathcal{K}(T_2) = \ln \mathcal{K}(T_1) + \int_{T_1}^{T_2} \frac{\Delta \mathcal{H}^{\circ}(T_1) + \Delta \mathcal{C}_{\rho}(T - T_1)}{\mathcal{R}T^2} dT$$

Over small \mathcal{T} ranges, $\Delta C_{\rho}(\mathcal{T} - \mathcal{T}_1)$ can be <u>assumed small</u> and $\Delta \mathcal{H}^{\circ}$ _independent of \mathcal{T}_i .

$$\Rightarrow \ln \mathcal{K}(\mathcal{T}_2) \approx \ln \mathcal{K}(\mathcal{T}_1) + \frac{\Delta \mathcal{H}^{\circ}}{\mathcal{R}} \left(\frac{1}{\mathcal{T}_1} - \frac{1}{\mathcal{T}_2}\right) = \ln \mathcal{K}(\mathcal{T}_1) + \frac{\Delta \mathcal{H}^{\circ}}{\mathcal{R}} \left(\frac{\mathcal{T}_2 - \mathcal{T}_1}{\mathcal{T}_1 \mathcal{T}_2}\right)$$

If
$$\Delta \mathcal{H}^{\circ}(\mathcal{T}) < 0$$
 (Exothermic) $\mathcal{T}_2 > \mathcal{T}_1$ means $\mathcal{K}_{\rho}(\mathcal{T}_2) < \mathcal{K}_{\rho}(\mathcal{T}_1)$
The equilibrium shifts toward reactants

If $\Delta \mathcal{H}^{\circ}(\mathcal{T}) > 0$ (Endothermic) $\mathcal{T}_{2} > \mathcal{T}_{1}$ means $\mathcal{K}_{\rho}(\mathcal{T}_{2}) > \mathcal{K}_{\rho}(\mathcal{T}_{1})$ The equilibrium shifts toward products

This is <u>Le Chatelier's principle for Temperature</u>

• <u>Example</u>: The Haber process

$$\frac{1}{2} N_2(g, T, p) + 3/2 H_2(g, T, p) = NH_3(g, T, p)$$
$$\Delta H^o_{rxn}(298 \text{ K}) = -46.21 \text{ kJ/mol}$$
$$\Delta G^o_{rxn}(298 \text{ K}) = -16.74 \text{ kJ/mol}$$

$$\mathcal{K}_{p} = \frac{\mathcal{P}_{\text{NH}_{3}}}{\mathcal{P}_{\text{H}_{2}}^{3/2} \mathcal{P}_{\text{N}_{2}}^{1/2}} = \mathcal{P}^{-1} \frac{\mathcal{X}_{\text{NH}_{3}}}{\mathcal{X}_{\text{H}_{2}}^{3/2} \mathcal{X}_{\text{N}_{2}}^{1/2}} = \mathcal{P}^{\frac{16,740 \text{ J/mol}}{(8.314 \text{ J/K-mol})(298 \text{ K})}} = 860$$

For p = 1 bar this is pretty good, lots of product. However, the reaction at room T is <u>slow</u> (this is kinetics, not thermodynamics). Raising T to 800 K can speed it up. But since $\Delta H^{\circ}(T) < 0$ (exothermic), Le Chatelier tells us that the equilibrium will shift toward the reactants.

Indeed: $K_{p}(800 \text{ K}) = 0.007$

What to do? \Rightarrow Note above $K_{\chi} = p K_{\rho}$

Again use Le Chatelier, but with pressure! If we increase p, Eq. shifts toward products.

 \Rightarrow Run reaction at high T and high p

For p = 1 bar, T = 800 K, $K_p = 0.007$

$$\mathcal{K}_{\chi} = \frac{\mathcal{X}_{\text{NH}_3}}{\mathcal{X}_{\text{H}_2}^{3/2} \mathcal{X}_{\mathcal{N}_2}^{1/2}} = (1) \mathcal{K}_{\rho} = 0.007$$

But at p = 100 bar, $K_{\chi} = (100)K_{p} = 0.7$ much better!

• <u>Heterogeneous Equilibria</u>

If a product or reactant is a <u>solid</u> or <u>liquid</u>, it will not appear in the ratio of partial p's for K_p or in the concentrations if the equilibrium is in solution. However, it must be used in ΔG .

Why? Take $v_A A(s) + v_B B(g) = v_C C(\ell) + v_D D(g)$

The solid and liquid are not mixed - they are pure states.

$$\Delta \boldsymbol{\mathcal{G}} = \left[\boldsymbol{v}_{\mathcal{C}} \boldsymbol{\mu}_{\mathcal{C}} \left(\boldsymbol{s}, \text{ pure}, \boldsymbol{p} \right) + \boldsymbol{v}_{\mathcal{D}} \boldsymbol{\mu}_{\mathcal{D}} \left(\boldsymbol{g}, \text{ mix}, \boldsymbol{p} \right) \right] - \left[\boldsymbol{v}_{\mathcal{A}} \boldsymbol{\mu}_{\mathcal{A}} \left(\boldsymbol{I}, \text{ pure}, \boldsymbol{p} \right) + \boldsymbol{v}_{\mathcal{B}} \boldsymbol{\mu}_{\mathcal{B}} \left(\boldsymbol{g}, \text{ mix}, \boldsymbol{p} \right) \right]$$

And for (ℓ) or (s) μ_{c} (pure, p) $\approx \mu^{\circ}$ (pure) (no *p*-dependence)

$$\Rightarrow \qquad \Delta \mathcal{G} = v_{\mathcal{C}} \mu_{\mathcal{C}}^{\circ} + v_{\mathcal{D}} \mu_{\mathcal{D}}^{\circ} - v_{\mathcal{A}} \mu_{\mathcal{A}}^{\circ} - v_{\mathcal{B}} \mu_{\mathcal{B}}^{\circ} + \mathcal{R} T \ln \frac{p_{\mathcal{D}}^{v_{\mathcal{D}}}}{p_{\mathcal{B}}^{v_{\mathcal{B}}}} = \Delta \mathcal{G}^{\circ} + \mathcal{R} T \ln \mathcal{Q}$$

$$\therefore \qquad \mathcal{K}_{p} = \left[\frac{\mathcal{P}_{D}^{\nu_{D}}}{\mathcal{P}_{B}^{\nu_{B}}}\right]_{Eq.} \qquad \underline{\text{No A or C involved}}.$$

But we still have

$$\Delta \mathcal{G}_{\mathsf{rxn}}^{\mathsf{o}} = v_{\mathcal{C}} \mu_{\mathcal{C}}^{\mathsf{o}} + v_{\mathcal{D}} \mu_{\mathcal{D}}^{\mathsf{o}} - v_{\mathcal{A}} \mu_{\mathcal{A}}^{\mathsf{o}} - v_{\mathcal{B}} \mu_{\mathcal{B}}^{\mathsf{o}}$$

and

$$\ln \mathcal{K}_{p} = -\frac{\Delta \mathcal{G}_{rxn}^{o}}{\mathcal{RT}}$$

e.g. the decomposition of limestone

$$CaCO_3(s) = CaO(s) + CO_2(g)$$
 T = 25°C

Calculate equilibrium vapor pressure at room T and elevated T. Data at 25°C:

Substance	$CaCO_3$ (s)	CaO (s)	CO ₂ (g)
μ° (kJ/mol)	-1128.8	-604.0	-394.36
$\Delta \overline{H}_{f}^{\circ}$ (kJ/mol)	-1206.9	-635.09	-393.51

At equilibrium,

$$\begin{split} \Delta \mathcal{G} &= \mu (CaO, s) + \mu (CO_2, g) - \mu (CaCO_3, s) \\ &= \mu^{\circ} (CaO, s) + \mu^{\circ} (CO_2, g) + RT \ln p_{CO_2} - \mu^{\circ} (CaCO_3, s) \\ &= \Delta \mathcal{G}^{\circ} + RT \ln \mathcal{K}_{\rho} \qquad \text{where} \quad \mathcal{K}_{\rho} = p_{CO_2} \text{ (at eq.)} \end{split}$$

The equilibrium constant includes only the gas, but ΔG° includes the solids too.

$$\Delta G^{\circ}$$
 (kJ/mol) = -604.0 - 394.4 - (-1128.8) = 130.4 kJ/mol
 ΔH° (kJ/mol) = -635.1 - 393.5 - (-1206.9) = 178.3 kJ/mol

Equilibrium pressure:

$$\ln K_{\rho} = -\frac{\Delta G^{\circ}}{RT} = -\frac{130,400 \text{ J/mol}}{(8.314 \text{ J/K-mol})(298.15 \text{ K})} = -52.50$$
$$K_{\rho} = 1.43 \times 10^{-23} \text{ bar}$$

Nothing there at room T! Try 1100 K:

$$\begin{aligned} \ln p_{CO_2} (1100 \text{ K}) &\approx \ln p_{CO_2} (298 \text{ K}) + \frac{\Delta \mathcal{H}^{\circ}}{R} \left(\frac{1}{1100 \text{ K}} - \frac{1}{298 \text{ K}} \right) \\ &= -52.50 - \frac{178,300 \text{ J/mol}}{8.314 \text{ J/K-mol}} \left(\frac{1}{1100 \text{ K}} - \frac{1}{298 \text{ K}} \right) = 0.17 \\ p_{CO_2} (1100 \text{ K}) &\approx 0.84 \text{ bar} \end{aligned}$$

There's probably some change in $\Delta \overline{H_f}^\circ$ over such a wide T range, but clearly the equilibrium shifts dramatically.