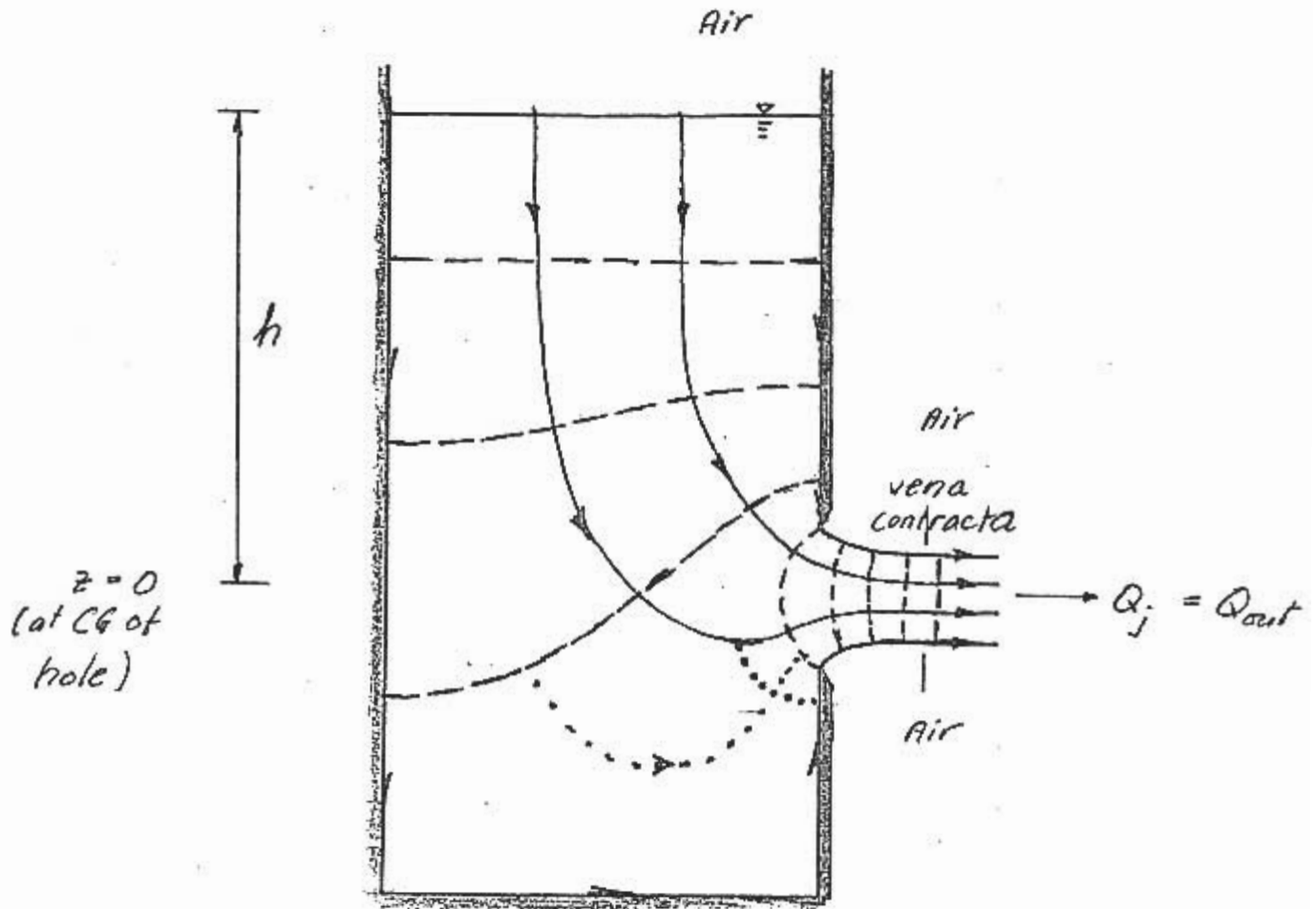


## RECITATION #4

### 1.060 ENGINEERING MECHANICS II

#### THERE'S A HOLE IN THE BUCKET

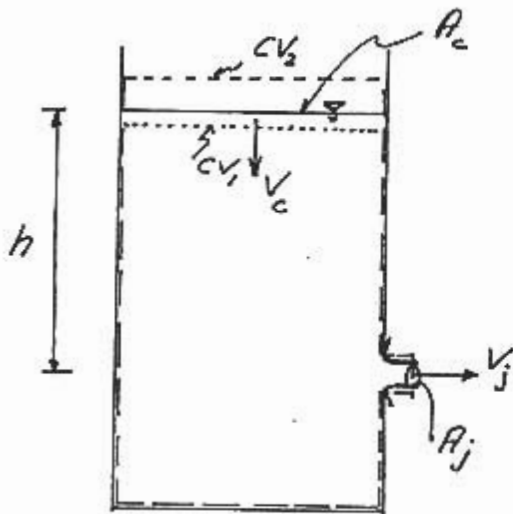
##### The Problem



Large container bucket : Surface Area  $A_c$   
Small hole in bucket : Hole Area  $A_h$   
Vena contracta jet : Area =  $A_j = C_v A_h$

How fast does water exit the bucket, or what is  $Q_j$  as the bucket is emptied?

# 1 Conservation of Volume (Continuity)



$CV_1$  has top surface just below free surface in bucket

$CV_2$  has top surface just above free surface in bucket

Otherwise,  $CV_1 = CV_2$

$CV_1$  is filled with water at all times. Conservation of volume (of water) within  $CV_1$  (it is constant) gives

$$\text{In} - \text{Out} = Q_{in} - Q_{out} = V_c A_c - V_j A_j = \text{change} = 0$$

$$V_c = (A_j / A_c) V_j \quad (1.1)$$

$CV_2$  does not have an inflow (of water), but volume of water inside  $CV_1$  changes with time. Conservation of volume gives

$$\text{In} - \text{Out} = -Q_{out} = -V_j A_j = \frac{d}{dt} (h A_c + \overset{\text{constant}}{V_0}) = A_c \frac{dh}{dt}$$

$$-\frac{dh}{dt} = (A_j / A_c) V_j \quad (1.2)$$

Since  $(-dh/dt)$  = velocity at which free surface is moving down, this must equal  $V_c$ , and (1.1) and (1.2) are one and the same!

## 2. Estimate of $V_j$ , the Outflow Velocity

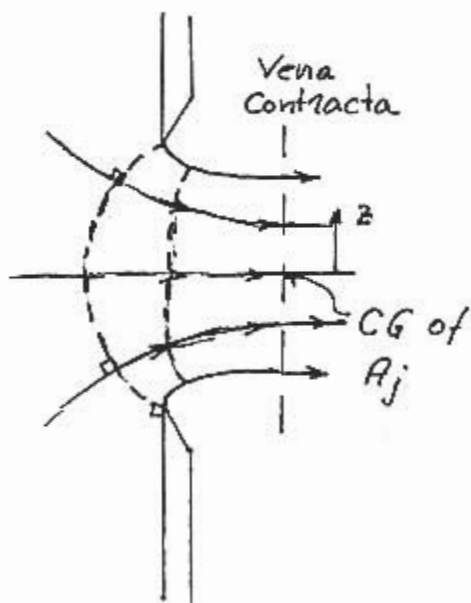
All streamlines must start at the free surface in the bucket and they must all pass the area,  $A_j$ , of the water jet shooting out of the hole in the bucket.

Along any streamline we have therefore from Bernoulli's equation [assuming flow to be steady]

$$\frac{1}{2} \rho V_j^2 + p_j + \rho g z_j = \frac{1}{2} \rho V_c^2 + p_c + \rho g z_c \quad (2.1)$$

From (1.1) we have  $V_c = (A_j/A_c)V_j$ , since streamline starts at free surface  $p_c = p_{atm} = 0$ , and choosing  $z=0$  at the center of gravity of  $A_j$  we have  $z_c = h$ . With this information, (2.1) may be written

$$V_j^2 (1 - (A_j/A_c)^2) = 2g(h - z_j) - 2p_j/\rho \quad (2.2)$$



In vicinity of the hole streamlines are curved, so pressure is not hydrostatic across the area of the hole in the bucket wall. However, after the flow has turned the corner the streamlines become straight (and parallel) at the so-called "vena contracta". Our control volume is chosen to cut across the jet at its "vena contracta".

First, these considerations suggest that

$$A_j = C_v A_h \quad (2.3)$$

in which  $A_h$  = area of the hole in the buckets wall, and  $C_v$  is a contraction coefficient. For circular holes  $C_v \approx 0.6$ , which is also the value for "plane" flow out of a long rectangular orifice.

Second observation from conditions at "vena contracta" is that the pressure is atmospheric all around the jet. With streamlines being straight line, there is no dynamic pressure ( $V^2/R$ ) inside the jet, so for any point on  $A_j$

$$p_j = 0 \quad (2.4)$$

Introducing these results in (2.2) gives

$$V_j^2 (1 - (C_v A_h / A_c)^2) = 2g(h - z_j) \quad (2.5)$$

in which  $z_j$  is the value of  $z$  for a particular streamline, as it passes  $A_j$  (vena contracta).

From (2.5) we finally obtain the velocity distribution across vena contracta

$$V_j = \sqrt{2gh} \frac{\sqrt{1 - z_j/h}}{\sqrt{1 - (C_v A_h / A_c)^2}} \quad (2.6)$$

First, we notice that accounting of the velocity,  $V_c$ , at the free surface of the bucket when specifying the Bernoulli constant has resulted in the factor

$$\sqrt{1 - (C_v A_h / A_c)^2} \approx 1 \quad (2.7)$$

for a hole that is reasonable small relative to the area of the bucket, e.g.  $A_h / A_c = 0.15$  [LARGE HOLE!] and  $C_v = 0.6$  gives the factor 0.996, which for all practical purposes is equal to unity.

Second, in order to obtain the discharge out of the bucket, we should really obtain this by integration over vena contracta, i.e.

$$Q_j = \int_{A_j} V_j dA = \sqrt{2gh} \int_{A_j} \sqrt{1 - z_j/h} dA \quad (2.8)$$

The integral is equal to  $A_j$  if we assume  $z_j/h \ll 1$ , but we can do better than that since for  $z_j/h$  reasonably small

$$\sqrt{1 - z_j/h} \approx 1 - \frac{1}{2} z_j/h$$

(e.g.  $z_j/h = 0.3$  gives  $\sqrt{0.7} = 0.84$  whereas the approximation gives 0.85. Not bad). With this approximation, the integral in (2.8) may be written

$$Q_j \approx \sqrt{2gh} \left( A_j - \frac{1}{2A_j} \int_{A_j} z_j dA \right) = \sqrt{2gh} A_j \quad (2.9)$$

by definition of the center of gravity of  $A_j$ , and having chosen this as our origin for  $z$ !

Equation (2.9) shows that the expression used for the outflow in the application of the continuity principle,

$$Q_j = V_j A_j = \sqrt{2gh} A_j$$

is an excellent approximation provided that we take

$$V_j = \sqrt{2gh} \quad (2.10)$$

with  $h$  being the vertical distance to the free surface in the bucket measured from the center of gravity of the hole in the bucket.

### 3. Effect of Unsteadiness

Introducing (2.10) in (1.2) we obtain an equation for the variation of surface level in the bucket as a result of the hole. This equation is

$$\frac{dh}{dt} = - \left( A_j / A_c \right) V_j = - \frac{C_v A_h}{A_c} \sqrt{2gh} = - K h^{1/2} \quad (3.1)$$

with  $K$  being a "constant" (with dimensions).

This equation is readily solved to give

$$\int_{h_0}^h h^{-\frac{1}{2}} dh = 2(\sqrt{h} - \sqrt{h_0}) = - \int_0^t K dt = -Kt$$

or

$$\sqrt{h} = \sqrt{h_0} - \frac{K}{2} t = \sqrt{h_0} - \frac{C_v A_h}{\sqrt{2} A_c} \sqrt{g} t \quad (3.2)$$

which may be used to estimate the length of time required to empty the bucket from its initial level,  $h = h_0$  at  $t = 0$ , to a lower level  $h$ . However, as  $h$  approaches zero, we must recall that our solution assumed, among other things,  $z_j / h \ll 1$  which is surely violated as  $h \rightarrow 0$ !

Equations (3.1) and (3.2) show that the flow we have considered based on the Bernoulli Equation for steady flow in fact is unsteady! Now, for an unsteady flow the Bernoulli equation is obtained from integration along a streamline

$$\int_{s_1}^{s_2} \frac{\partial}{\partial s} \left[ \frac{1}{2} \rho V_s^2 + p_s + \rho g z_s \right] ds = - \int_{s_1}^{s_2} \rho \frac{\partial V_s}{\partial t} ds \quad (3.3)$$

or, for our problem, with  $s_1 = s_c = 0$  at the surface in the bucket and  $s_2 = s_j$  at vena contracta, we have

$$V_j^2 (1 - (A_j/A_c)^2) = 2gh (1 - \frac{z_j}{h}) - 2 \int_{s_c}^{s_j} (\partial V_s / \partial t) ds \quad (3.4)$$

Without unsteady effects we obtained

$$V_j = \sqrt{2gh}$$

so

$$\partial V_j / \partial t = \frac{1}{2} \sqrt{2g} h^{-\frac{1}{2}} \frac{\partial h}{\partial t} = \sqrt{2gh} \frac{-V_c}{2h} = -2gh \left( \frac{A_j}{A_c} \right) \frac{1}{2h} \quad (3.5)$$

represents the maximum acceleration ( $V_j \gg V_s$ ) along any streamline from the surface in the bucket to vena contracta. At the start of the streamline, at the free surface in the bucket, we have

$$\frac{\partial V_c}{\partial t} = \left( \frac{A_j}{A_c} \right) \frac{\partial V_j}{\partial t} = -2gh \left( \frac{A_j}{A_c} \right)^2 \frac{1}{2h} \quad (3.6)$$

which represents a minimum value of  $\partial V_s / \partial t$ .

By (3.5) and (3.6), with the length of any streamline  $s_j - s_c = h$ , we obtain from (3.4)

$$V_j^2 \left( 1 - \left( \frac{A_j}{A_c} \right)^2 \right) = 2gh \left[ \left( 1 - \frac{z_j}{h} \right) + \left\{ \frac{A_j}{A_c} \right\} \right] \quad (3.7)$$

which shows the effect of unsteady flow to increase the predicted velocity at vena contracta by a factor,  $F_u$ , bounded by

$$\sqrt{1 + \left( \frac{A_j}{A_c} \right)^2} < F_u < \sqrt{1 + A_j / A_c} \quad (3.8)$$

with  $F_u$  most likely closer to the lower than to the higher bound.



#### 4. General Conclusions

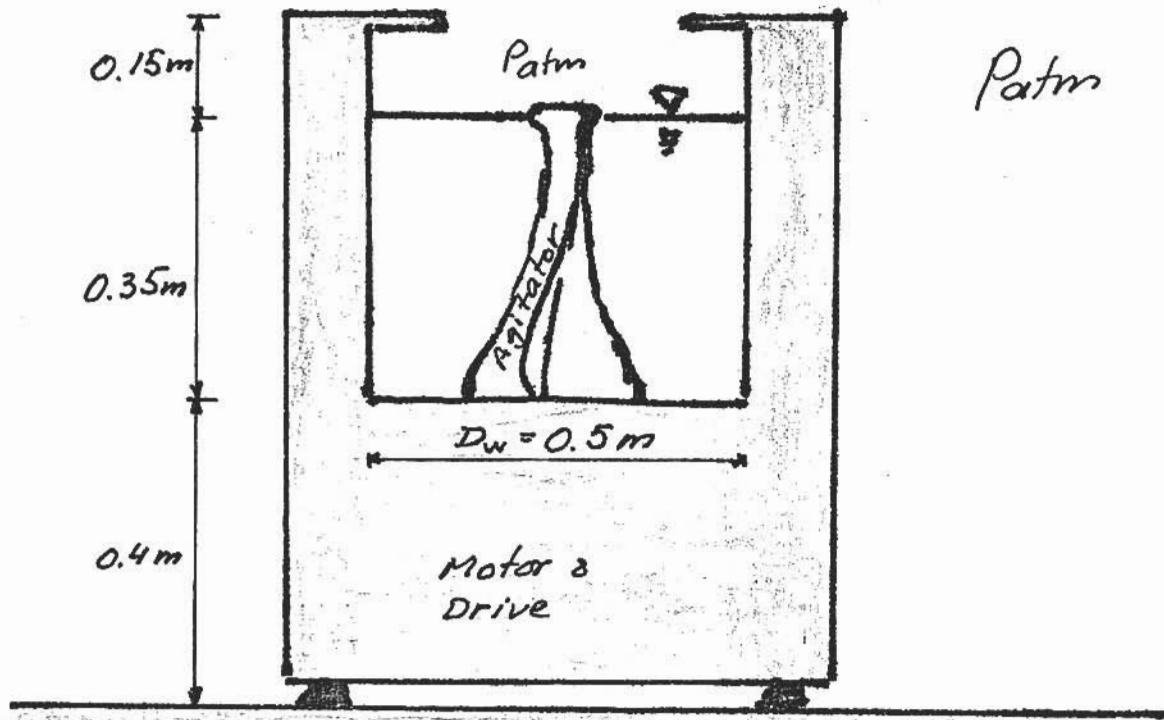
For converging flows from a large crosssection to a small crosssection one may

- Neglect the velocity in the large crosssection when evaluating the Bernoulli constant.
- Choose origin of  $z$  at center of gravity, CG, of small crosssectional area  $A_{small}$
- Evaluate velocity from streamline passing through CG of  $A_{small}$ , and obtain discharge by multiplying this velocity and  $A_{small}$ .
- Neglect unsteady effects in Bernoulli's equation.

In all cases, when in doubt, check assumptions' validity. This note should provide you with a useful example of how one may proceed to check the validity of the above assumptions.

## RECITATION # 4

### Problem NO: 1



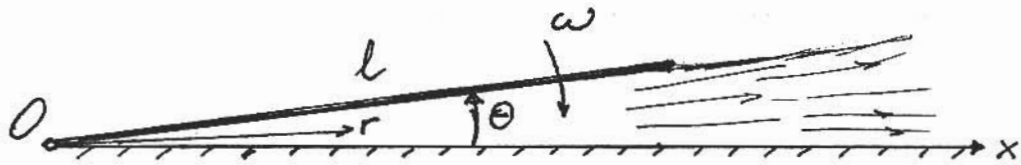
Your washer breaks down just after completing the hot washing cycle. You need to get rid of the hot water in order to examine the situation and find out what went/is wrong with the washer.

You have a 10ft long,  $\frac{1}{2}$  inch (diameter) 10ft long rubber hose, a standard bucket, and a floor drain located 3ft. from the washer.

How are you going to get rid of the hot water, and how long will it take? (treat water as incompressible & inviscid)

## Problem No: 2

Palm



A plate of length  $l$  (very long into paper, so problem may be treated as 2-D) rotates around a pivot point,  $O$ , at an angular velocity  $\omega$  [rad/s] forcing the plate down towards a horizontal surface. The angle between the rotating plate and the surface,  $\theta$ , is decreasing with time and water filling the gap is being squeezed out.  $\theta \ll 1$  [rad] so  $\sin \theta = \tan \theta = \theta$ ,  $\cos \theta = 1$ .

Treat fluid as incompressible and inviscid.

- 1) Determine the velocity in the gap as a function of radial distance  $r$  from  $O$ , (since  $\cos \theta = 1$  you call ~~it~~  $x$  or  $r$ , up to you),  $\theta$  and  $\omega$ .
- 2) Assuming steady flow and neglecting elevation differences (take  $z = 0$  everywhere) determine the pressure variation, <sub>px</sub> along the plate.

(over)

- 3) Integrate  $p(r)$  obtained in (2) along the length of the plate  $L$  to obtain the total pressure force (per unit length into paper),  $P_p$ , acting on the plate, its direction and vertical component.
- 4) For  $L = 8\text{ cm}$ ,  $\omega = 100\text{ rad/s}$ ,  $\rho = 1,000\text{ kg/m}^3$ , evaluate the force  $P_p$  obtained in (3) for  $\theta = 15^\circ$  and  $7^\circ$ .
- 5) If you were to account for unsteadiness would you expect this to be important? and would it increase or decrease your estimate of  $P_p$ ?
- 6) If you were to account for frictional forces along plate and horizontal surface, would  $P_p$  increase or decrease?

## RECITATION #4

### Problem NO: 1

- 1) Submerge the rubber hose in the hot water in the washing machine so that it is completely full of water.
- 2) Close one end of rubber hose with your thumb and lift it out of washing machine and locate it above the floor drain. During this operation, the other end of the hose should remain submerged in the washing machine.

You have primed the siphon - let go with the thumb and water will start running.

### Velocity in hose

Use Bernoulli from washing machine to floor drain

$$H_w = \text{head in washer} = z_w + \frac{P_w}{\rho g} + \frac{V_w^2}{2g} =$$
$$0.4 + h + 0 = \text{head at inflow to hose}$$

( $z=0$  at floor level,  $h$  = depth of water in washer,  $V_w$  = velocity of water in washer  $\approx 0$  because of the large flow area).

$$H_{fd} = \text{head at floor drain} = \frac{P_{atm}}{\rho g} + z_{fd} + \frac{V_h^2}{2g}$$

"0"                      "0"                      "0"

$$V_h = \text{velocity in hose} = \sqrt{2g(h+0.4)} \quad (SI)$$

## Discharge

$$Q_h = \text{discharge in hose} = V_h \cdot \frac{\pi}{4} d_h^2 =$$

$$\sqrt{2g(h+0.4)} \cdot \frac{\pi}{4} (0.0127)^2 = 5.6 \cdot 10^{-4} \sqrt{h+0.4} \text{ (SI)}$$

## Conservation of Volume

$$-\frac{\partial h}{\partial t} \left( \frac{\pi}{4} D_w^2 - \text{area of agitator} \right) = Q_h$$

or

$$\frac{dh}{dt} = \frac{Q_h}{\frac{\pi}{4} \cdot 0.5^2} = -2.9 \cdot 10^{-3} \sqrt{h+0.4}$$

or

$$\frac{dh/dt}{\sqrt{h+0.4}} = -2.9 \cdot 10^{-3} \Rightarrow \frac{dh}{\sqrt{h+0.4}} = -2.9 \cdot 10^{-3} dt$$

Integrate from  $t=0$  ( $h=0.35\text{m}$ ) to  $t$  ( $h=h$ )  
to get

$$\left[ 2\sqrt{h+0.4} \right]_{0.35}^h = 2(\sqrt{h+0.4} - \sqrt{0.35+0.4}) =$$

$$2(\sqrt{h+0.4} - \sqrt{0.75}) = -2.9 \cdot 10^{-3} t$$

$h=0$  - washing machine is empty -  
and

$$t_{\text{empty}} \cong \frac{2(\sqrt{0.75} - \sqrt{0.4})}{2.9 \cdot 10^{-3}} = 16/\text{sec} \approx \underline{2 \text{ to } 3 \text{ min}}$$

## RECITATION #4

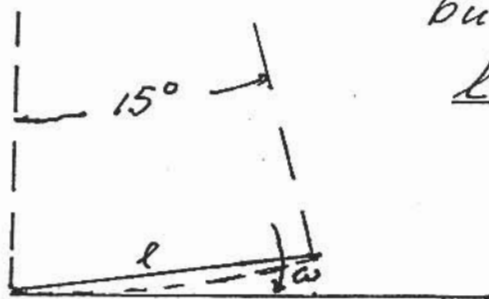
### Problem No: 2

$r = 30 \text{ cm} \approx$  radius of a car's wheel

$V_c = 65 \text{ mph} = 29 \text{ m/s} =$  speed of the car

$V_c \cdot T = 2\pi r \Rightarrow \underline{\omega} = \text{rad. freq. of wheel} = V_c / r \approx \underline{100 \frac{\text{rad}}{\text{s}}}$

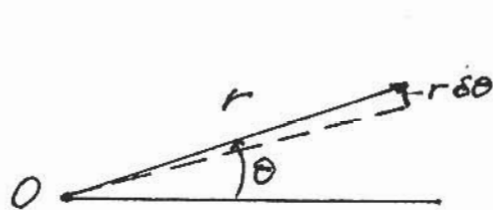
Circular wheel approximated by  $24$  sided polygon -  $360/24 = 15^\circ = 0.26 \text{ rad.} \Rightarrow$  Bumpy ride, but simpler to analyse.



$$\underline{l} \approx r \sin 15^\circ = \underline{7.8 \text{ cm}}$$

Our problem simulates a tire hitting the road when it is covered by a layer of water.

### Conservation of Volume



$$Q_{in} - Q_{out} = 0 - V(r) r \theta =$$

$$\frac{\partial V}{\partial t} = \frac{\frac{1}{2} r \cdot r \delta \theta}{\delta t} = \frac{\frac{1}{2} r^2 (-\omega \delta t)}{\delta t} = -\frac{1}{2} r^2 \omega$$

$$\underline{V(r) = \frac{1}{2} r \omega \theta^{-2}}$$

Note:

$$\frac{\partial V(r)}{\partial t} = \frac{1}{2} r \omega (-\theta^{-2}) \frac{d\theta}{dt} = \frac{1}{2} r \omega^2 \theta^{-2}$$

## Bernoulli (general)

$$\int_r^{\ell} \rho \frac{\partial V(r)}{\partial t} dr + \left[ \frac{1}{2} \rho V(r)^2 + p(r) + \rho g z \right]_r^{\ell} = 0$$

or

$$\int_r^{\ell} \rho \frac{\partial V(r)}{\partial t} dr + \frac{1}{2} \rho V_{\ell}^2 + p_{\ell} = \frac{1}{2} \rho V(r)^2 + p(r)$$

With  $p_{\ell} = p_{atm} = 0$  and

$$V(r) = \frac{1}{2} r \omega \theta^{-1}, \quad V_{\ell} = \frac{1}{2} \ell \omega \theta^{-1}$$

$$p(r) = \frac{1}{8} \rho \left( \frac{\omega}{\theta} \right)^2 (\ell^2 - r^2) + \int_r^{\ell} \rho \frac{1}{2} r \left( \frac{\omega}{\theta} \right)^2 dr =$$
$$\frac{1}{8} \rho \left( \frac{\omega}{\theta} \right)^2 \ell^2 \left( 1 - \left( \frac{r}{\ell} \right)^2 \right) + \frac{1}{4} \rho \left( \frac{\omega}{\theta} \right)^2 \ell^2 \left( 1 - \left( \frac{r}{\ell} \right)^2 \right)$$

Note: Unsteady effect on  $p(r)$  is TWICE  
the value of steady result!

$$p(r) = \frac{1}{8} \rho \left( \frac{\omega \ell}{\theta} \right)^2 \left( 1 - \left( \frac{r}{\ell} \right)^2 \right) \cdot \begin{cases} 1 & \text{if steady only} \\ 3 & \text{if unsteady included!} \end{cases}$$

Total Pressure Force (per unit length into paper)

$$P_p = \int_0^{\ell} p(r) dr = \ell \int_0^1 \frac{1}{8} \rho \left( \frac{\omega \ell}{\theta} \right)^2 \left( 1 - \left( \frac{r}{\ell} \right)^2 \right) d\left( \frac{r}{\ell} \right) \cdot \begin{cases} 1 & \text{St} \\ 3 & \text{US.} \end{cases} =$$

$$\frac{1}{12} \rho \left( \frac{\omega \ell}{\theta} \right)^2 \ell \begin{cases} 1 & \text{St.} \\ 3 & \text{US.} \end{cases}$$

Directed upwards,  
perpendicular to plate  $\approx$  Vertical since  $\cos \theta \approx 1$ .



## Evaluation of Force on a Tire

$$L = 7.8 \text{ cm} = 0.078 \text{ m}; \quad \omega = 100 \text{ rad/s}; \quad \rho = 1,000 \frac{\text{kg}}{\text{m}^3}$$

$$P_f = 395 \cdot \theta^{-2} \cdot \begin{cases} 1 \text{ St.} \\ 3 \text{ USt.} \end{cases} \quad \text{N/m if } \theta \text{ in rad.}$$

With width of tire (into paper)  $b = 20 \text{ cm} = 0.2 \text{ m}$   
we have

$$\underline{P_{up} = P_f \cdot 0.2 = 79 \theta^{-2} \begin{cases} 1 \text{ St.} \\ 3 \text{ USt.} \end{cases} \text{ N.}}$$

Weight of a Car  $\approx 1,000 \cdot 9.8 = 10^4 \text{ N}$

Force per wheel  $\sim 2.5 \cdot 10^3 \text{ N}$  to overcome gravity

$$P_{up} = 79 \theta_{cr}^{-2} \begin{cases} 1 \text{ St.} \\ 3 \text{ USt.} \end{cases} = 2.5 \cdot 10^3$$

gives

$$\theta_{cr}^2 = \frac{79}{2.5 \cdot 10^3} \begin{cases} 1 \text{ St.} \\ 3 \text{ USt.} \end{cases} \Rightarrow \underline{\theta_{cr} = \begin{cases} 0.177 \text{ St.} \\ 0.308 \text{ USt.} \end{cases}}$$

For any value of  $\theta < \theta_{cr}$  the uplift force on a smooth tire hitting a smooth water-covered surface at a speed of  $V_c = 65 \text{ mph}$  will exceed gravity, i.e. there is no contact force between tire and road. Car is hydroplaning! Now you know why tires have  $\neq$  treads and why auto races stop whenever it rains.